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Composition comprising EPDM and a paraffinic oil

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COMPOSITION COMPRISING EPDM AND A PARAFFINIC OIL

The invention is directed to a composition comprising an ethylene-propylene-diene (EPDM) rubber component and a paraffinic oil component.

Such a EPDM containing compositions are well known and are described in detail in Rubber Technology Handbook, Werner Hofmann, Oxford University Press, New York, 1980, paragraph 3.3.8, pages 93-100. Paraffinic oils are used as plasticisers or softening agent in such compositions. Also compositions often referred to as thermoplastic elastomers (TPE) or also sometimes referred to as thermoplastic vulcanisates (TPV) as described in said Handbook on pages 144 - 150 and 154 - 156 comprising EPDM and a polypropylene may comprise paraffinic process oils. Examples of such compositions may be found in EP-A-1132242, GB-A-155020, US-A-5290886 and EP-A-1028145.

The paraffinic oils commonly used in such applications are either hydroprocessed petroleum derived oils, such as the Paralux oils as supplied by Chevron Products Company or synthetic paraffin oils, for example poly-alpha olefins such as a low weight component of Poly- ethylene-propylene such as described in EP-A-1028145.

Compositions as described above are often used in automotive applications, such as parts of the interior of the automobile. There is an increasing demand for low hydrocarbon emissions of an automobile. These hydrocarbon emissions are measured by keeping a

complete car at an elevated temperature and detecting any hydrocarbon emissions. In view of this development there is an increasing demand for EPDM containing compositions having a low hydrocarbon emission.

5 The object of this invention is to provide an EPDM containing composition having a low hydrocarbon emission.

10 This object is achieved by the following composition. A composition comprising an ethylene-propylene-diene (EPDM) rubber component and a paraffinic oil component, wherein the paraffinic oil component is a Fischer-Tropsch derived process oil.

15 Applicants have found that a process oil as derived from a Fischer-Tropsch synthesis product can be simply obtained having properties which lower the hydrocarbon emissions of the finished EPDM comprising product. Some severely hydroprocessed or synthetic paraffinic process oils as described above may also achieve this lower hydrocarbon emission. A disadvantage of these products is that they are either very expensive because they have to be synthesized from lower olefins or heavily hydroprocessed. Another advantage of the Fischer-Tropsch derived oils as compared to the heavily hydroprocessed oils is that the low temperature properties for the higher viscosity grade oils is much better making the Fischer-Tropsch derived oils more easy to handle in the process to make the EPDM containing product.

25 The Fischer-Tropsch derived oil preferably has a flash point according to ISO 2592 of above 240 °C and more preferably above 260 °C. The UV adsorption of the oil at 300 nm is preferably less than 1% and more preferably less than 0.6% according to ASTM D 2008-A1. The evaporation loss at 107 °C during 22 hours of the oil (according to ASTM D 972 is preferably less than 0.1 wt%

30

and more preferably less than 0.05 wt%.

5 The kinematic viscosity at 100 °C of the oil will be resultant from the above requirements and will usually be above 8 cSt and more preferably above 9 cSt. The upper limit is not essential for the hydrocarbon emissions requirements. Nevertheless it is not advantageous to use too viscous oil for practical processing reasons. Preferably the upper limit will be around 30 cSt, preferably 25 cSt. The pour point of the process oil will be dependent on the viscosity grade used. Applicants have found a process involving a catalytic dewaxing step to prepare a Fischer-Tropsch process oil having pour points ranging from - 40 °C for the less viscous grades to around 10 °C for the more viscous grades. This has been found very advantageous because the oil can be used in a liquid state at ambient conditions during the manufacturing of the EPDM comprising composition. Applicants further found that the Fischer-Tropsch derived oil preferably has a CN number as measured according to IEC 590 of between 15 and 30%.

20 The process oil is preferably prepared using the below process, by

(a) hydrocracking/hydroisomerising a feed comprising a Fischer-Tropsch derived feed,

25 (b) isolating from the product of step (a) a process oil precursor fraction,

(c) dewaxing the process oil precursor fraction obtained in step (b) to obtain the process oil, optionally after separating a lower boiling fraction from said dewaxed product.

30 The Fischer-Tropsch derived feed can be obtained by well-known processes, for example the so-called commercial Sasol process, the commercial Shell Middle

Distillate Process or by the non-commercial Exxon process. These and other processes are for example described in more detail in EP-A-776959, EP-A-668342, US-A-4943672, US-A-5059299, WO-A-9934917 and WO-A-9920720.

5 A preferred process to prepare the process oil having the desired flash point, evaporation loss and CN-number properties involves using a Fischer-Tropsch derived feed in step (a) which is characterized in that the weight
10 ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms in the Fischer-Tropsch derived feed is at least 0.2 and wherein at least 30 wt% of compounds in the Fischer-Tropsch product have at least 30 carbon atoms.
15 More preferably the feed has at least 50 wt% and most preferably at least 55 wt% of compounds having at least 30 carbon atoms. Furthermore the weight ratio of compounds having at least 60 or more carbon atoms and compounds having at least 30 carbon atoms of the
20 Fischer-Tropsch derived feed is preferably at least 0.4 and more preferably at least 0.55. The Fischer-Tropsch derived feed is preferably derived from a Fischer-Tropsch product which comprises a C₂₀+ fraction having an ASF-alpha value (Anderson-Schulz-Flory chain
25 growth factor) of at least 0.925, preferably at least 0.935, more preferably at least 0.945, even more preferably at least 0.955.

30 The initial boiling point of the Fischer-Tropsch derived feed may range up to 400 °C, but is preferably below 200 °C. Preferably at least any compounds having 4 or less carbon atoms and any compounds having a boiling point in that range are separated from a Fischer-Tropsch synthesis product before the

Fischer-Tropsch synthesis product is used as a Fischer-Tropsch derived feed in step (a). In addition to this Fischer-Tropsch product also other fractions may be part of the Fischer-Tropsch derived feed. Possible other fractions may suitably be any high boiling fraction obtained in step (b).

Such a Fischer-Tropsch derived feed is suitably obtained by a Fischer-Tropsch process, which yields a relatively heavy Fischer-Tropsch product. Not all Fischer-Tropsch processes yield such a heavy product. An example of a suitable Fischer-Tropsch process is described in WO-A-9934917 and in AU-A-698392. These processes may yield a Fischer-Tropsch product as described above.

The Fischer-Tropsch derived feed and the resulting waxy raffinate product will contain no or very little sulphur and nitrogen containing compounds. This is typical for a product derived from a Fischer-Tropsch reaction, which uses synthesis gas containing almost no impurities. Sulphur and nitrogen levels will generally be below the detection limits, which are currently 5 ppm for sulphur and 1 ppm for nitrogen

The Fischer-Tropsch product may optionally be subjected to a mild hydrotreatment step in order to remove any oxygenates and saturate any olefinic compounds present in the reaction product of the Fischer-Tropsch reaction. Such a hydrotreatment is described in EP-B-668342. The mildness of the hydrotreating step is preferably expressed in that the degree of conversion in this step is less than 20 wt% and more preferably less than 10 wt%. The conversion is here defined as the weight percentage of the feed boiling above 370 °C that reacts to a fraction boiling below 370 °C. After such a mild

hydrotreatment lower boiling compounds, having three or less carbon atoms and other compounds boiling in that range, will preferably be removed from the effluent before it is used in step (a).

5 The hydrocracking/hydroisomerisation reaction of step (a) is preferably performed in the presence of hydrogen and a catalyst, which catalyst can be chosen from those known to one skilled in the art as being suitable for this reaction. Catalysts for use in step (a)
10 typically comprise an acidic functionality and a hydrogenation/dehydrogenation functionality. Preferred acidic functionalities are refractory metal oxide carriers. Suitable carrier materials include silica, alumina, silica-alumina, zirconia, titania and mixtures thereof. Preferred carrier materials for inclusion in the
15 catalyst for use in the process of this invention are silica, alumina and silica-alumina. A particularly preferred catalyst comprises platinum supported on a silica-alumina carrier. If desired, the acidity of the
20 catalyst carrier may be enhanced by applying a halogen moiety, in particular fluorine, or a phosphorous moiety to the carrier. Examples of suitable hydrocracking/hydro-isomerisation processes and suitable catalysts are described in WO-A-0014179, EP-A-532118 and
25 the earlier referred to EP-A-776959.

30 Preferred hydrogenation/dehydrogenation functionalities are Group VIII metals, such as nickel, cobalt, iron, palladium and platinum. Preferred are the noble metal Group VIII members, palladium and more preferred platinum. The catalyst may comprise the more preferred noble metal hydrogenation/dehydrogenation active component in an amount of from 0.005 to 5 parts by weight, preferably from 0.02 to 2 parts by weight,

per 100 parts by weight of carrier material.

A particularly preferred catalyst for use in the hydroconversion stage comprises platinum in an amount in the range of from 0.05 to 2 parts by weight, more preferably from 0.1 to 1 parts by weight, per 100 parts by weight of carrier material. The catalyst may also comprise a binder to enhance the strength of the catalyst. The binder can be non-acidic. Examples are clays and other binders known to one skilled in the art.

In step (a) the feed is contacted with hydrogen in the presence of the catalyst at elevated temperature and pressure. The temperatures typically will be in the range of from 175 to 380 °C, preferably higher than 250 °C and more preferably from 300 to 370 °C. The pressure will typically be in the range of from 10 to 250 bar and preferably between 20 and 80 bar. Hydrogen may be supplied at a gas hourly space velocity of from 100 to 10000 Nl/l/hr, preferably from 500 to 5000 Nl/l/hr. The hydrocarbon feed may be provided at a weight hourly space velocity of from 0.1 to 5 kg/l/hr, preferably higher than 0.5 kg/l/hr and more preferably lower than 2 kg/l/hr. The ratio of hydrogen to hydrocarbon feed may range from 100 to 5000 Nl/kg and is preferably from 250 to 2500 Nl/kg.

The conversion in step (a) as defined as the weight percentage of the feed boiling above 370 °C which reacts per pass to a fraction boiling below 370 °C, is at least 20 wt%, preferably at least 25 wt%, but preferably not more than 80 wt%, more preferably not more than 65 wt%. The feed as used above in the definition is the total hydrocarbon feed fed to step (a), thus also any optional

recycle of the higher boiling fraction as obtained in step (b).

In step (b) the product of step (a) is preferably separated into one or more distillate fractions, a process oil precursor fraction, preferably having a T10wt% boiling point of between 300 and 450 °C. A heavy fraction may be separated from the product of step (a) to adjust the resultant viscosity of the process oil. If no heavy fraction is removed the kinematic viscosity at 100 °C of the process oil may be well above 15 cSt. By adjusting the amount and cut point at which the said heavy fraction is separated from the effluent of step (a) process oils can be obtained having a kinematic viscosity at 100 °C ranging from 8 cSt cSt to above 25 cSt.

In step (c) the process oil precursor fraction obtained in step (b) is subjected to a dewaxing treatment wherein the pour point of the oil is reduced. The pour point is preferably reduced by more than 10 °C. Dewaxing can be performed by means of a so-called solvent dewaxing process or by means of a catalytic dewaxing process.

Solvent dewaxing is well known to those skilled in the art and involves admixture of one or more solvents and/or wax precipitating agents with the process oil precursor fraction and cooling the mixture to a temperature in the range of from - 10 °C to - 40 °C, preferably in the range of from - 20 °C to - 35 °C, to separate the wax from the oil. The oil containing the wax is usually filtered through a filter cloth which can be made of textile fibres, such as cotton; porous metal cloth; or cloth made of synthetic materials. Examples of solvents which may be employed in the solvent dewaxing process are C₃-C₆ ketones (e.g. methyl ethyl ketone,

methyl isobutyl ketone and mixtures thereof),
C₆-C₁₀ aromatic hydrocarbons (e.g. toluene),
mixtures of ketones and aromatics (e.g. methyl ethyl
ketone and toluene), autorefrigerative solvents such as
5 liquefied, normally gaseous C₂-C₄ hydrocarbons such as
propane, propylene, butane, butylene and mixtures
thereof. Mixtures of methyl ethyl ketone and toluene or
methyl ethyl ketone and methyl isobutyl ketone are
generally preferred. Examples of these and other suitable
10 solvent dewaxing processes are described in Lubricant
Base Oil and Wax Processing, Avilino Sequeira, Jr.,
Marcel Dekker Inc., New York, 1994, Chapter 7.

Preferably step (c) is performed by means of a
catalytic dewaxing process. The catalytic dewaxing
15 process can be performed by any process wherein in the
presence of a catalyst and hydrogen the pour point of the
process oil precursor fraction is reduced as specified
above. Suitable dewaxing catalysts are heterogeneous
catalysts comprising a molecular sieve and optionally in
20 combination with a metal having a hydrogenation function,
such as the Group VIII metals. Molecular sieves, and more
suitably intermediate pore size zeolites, have shown a
good catalytic ability to reduce the pour point of the
process oil precursor fraction under catalytic dewaxing
25 conditions. Preferably the intermediate pore size
zeolites have a pore diameter of between 0.35 and 0.8 nm.
Suitable intermediate pore size zeolites are mordenite,
ZSM-5, ZSM-12, ZSM-22, ZSM-23, SSZ-32, ZSM-35 and ZSM-48.
Another preferred group of molecular sieves are the
30 silica-aluminaphosphate (SAPO) materials of which SAPO-11
is most preferred as for example described in
US-A-4859311. ZSM-5 may optionally be used in its HZSM-5
form in the absence of any Group VIII metal. The other

molecular sieves are preferably used in combination with an added Group VIII metal. Suitable Group VIII metals are nickel, cobalt, platinum and palladium. Examples of possible combinations are Ni/ZSM-5, Pt/ZSM-23, Pd/ZSM-23, Pt/ZSM-48 and Pt/SAPO-11. Further details and examples of suitable molecular sieves and dewaxing conditions are for example described in WO-A-9718278, US-A-5053373, US-A-5252527 and US-A-4574043.

The dewaxing catalyst suitably also comprises a binder. The binder can be a synthetic or naturally occurring (inorganic) substance, for example clay, silica and/or metal oxides. Natural occurring clays are for example of the montmorillonite and kaolin families. The binder is preferably a porous binder material, for example a refractory oxide of which examples are: alumina, silica-alumina, silica-magnesia, silica-zirconia, silica-thoria, silica-beryllia, silica-titania as well as ternary compositions for example silica-alumina-thoria, silica-alumina-zirconia, silica-alumina-magnesia and silica-magnesia-zirconia. More preferably a low acidity refractory oxide binder material, which is essentially free of alumina, is used. Examples of these binder materials are silica, zirconia, titanium dioxide, germanium dioxide, boria and mixtures of two or more of these of which examples are listed above. The most preferred binder is silica.

A preferred class of dewaxing catalysts comprise intermediate zeolite crystallites as described above and a low acidity refractory oxide binder material which is essentially free of alumina as described above, wherein the surface of the aluminosilicate zeolite crystallites has been modified by subjecting the aluminosilicate zeolite crystallites to a surface dealumination

treatment. A preferred dealumination treatment is by contacting an extrudate of the binder and the zeolite with an aqueous solution of a fluorosilicate salt as described in for example US-A-5157191 or WO-A-0029511.

5 Examples of suitable dewaxing catalysts as described above are silica bound and dealuminated Pt/ZSM-5, silica bound and dealuminated Pt/ZSM-23, silica bound and dealuminated Pt/ZSM-12, silica bound and dealuminated Pt/ZSM-22, as for example described in WO-A-0029511 and
10 EP-B-832171.

Catalytic dewaxing conditions are known in the art and typically involve operating temperatures in the range of from 200 to 500 °C, suitably from 250 to 400 °C, hydrogen pressures in the range of from 10 to 200 bar,
15 preferably from 40 to 70 bar, weight hourly space velocities (WHSV) in the range of from 0.1 to 10 kg of oil per litre of catalyst per hour (kg/l/hr), suitably from 0.2 to 5 kg/l/hr, more suitably from 0.5 to 3 kg/l/hr and hydrogen to oil ratios in the range of from
20 100 to 2,000 litres of hydrogen per litre of oil. By varying the temperature between 315 and 375 °C at between 40-70 bars, in the catalytic dewaxing step it is possible to prepare base oils having different pour point specifications varying from suitably - 10 to - 60 °C.

25 Optionally a lower boiling fraction is separated from the oil as obtained after dewaxing. The need to separate a fraction will be determined by the properties of the process oil precursor fraction used in step (c) and the dewaxing process used. For example a catalytic dewaxing
30 step will suitably require such a separation because lower boiling fractions are formed in the dewaxing process, which need to be removed in order to achieve the

volatility requirements of the process oil used in the present invention.

5 The process oil may be subjected to a hydrofinishing step or an adsorption step in order to improve its colour properties. Adsorption may be performed by contacting the oil with a suitable heterogeneous adsorbents, for example active carbon, zeolites, for example natural faujasite, or synthetic materials such as ferrierite, ZSM-5, faujasite, mordenite, metal oxides such as silica powder, silica gel, aluminum oxide and various clays, 10 for example Attapulgus clay (hydrous magnesium-aluminium silicate), Porocel clay (hydrated aluminium oxide). A preferred adsorbent is activated carbon.

15 A hydrofinishing step is suitably carried out at a temperature between 180 and 380 °C, a total pressure of between 10 to 250 bar and preferably above 100 bar and more preferably between 120 and 250 bar. The WHSV (Weight hourly space velocity) ranges from 0.3 to 2 kg of oil per litre of catalyst per hour (kg/l.h).

20 The hydrogenation catalyst is suitably a supported catalyst comprising a dispersed Group VIII metal. Possible Group VIII metals are cobalt, nickel, palladium and platinum. Cobalt and nickel containing catalysts may also comprise a Group VIB metal, suitably molybdenum and tungsten. Suitable carrier or support materials are 25 amorphous refractory oxides. Examples of suitable amorphous refractory oxides include inorganic oxides, such as alumina, silica, titania, zirconia, boria, silica-alumina, fluorided alumina, fluorided silica-alumina and mixtures of two or more of these. 30

Examples of suitable hydrogenation catalysts are nickel-molybdenum containing catalyst such as KF-847 and KF-8010 (AKZO Nobel) M-8-24 and M-8-25 (BASF), and C-424,

DN-190, HDS-3 and HDS-4 (Criterion); nickel-tungsten containing catalysts such as NI-4342 and NI-4352 (Engelhard) and C-454 (Criterion); cobalt-molybdenum containing catalysts such as
5 KF-330 (AKZO-Nobel), HDS-22 (Criterion) and HPC-601 (Engelhard). Preferably platinum containing and more preferably platinum and palladium containing catalysts are used. Preferred supports for these palladium and/or platinum containing catalysts are
10 amorphous silica-alumina. Examples of suitable silica-alumina carriers are disclosed in WO-A-9410263. A preferred catalyst comprises an alloy of palladium and platinum preferably supported on an amorphous silica-alumina carrier of which the commercially
15 available catalyst C-624 and C-654 of Criterion Catalyst Company (Houston, TX) are examples.

The content of the Fischer-Tropsch derived paraffinic process oil in the composition according to the present invention will depend on the desired properties of the
20 end product and on the other components of the composition. The oil is usually applied as plasticiser. Typical ranges are mentioned in the above referred to patent applications. Typically the content of the paraffinic process oil may be between 1 and 60 wt% of the
25 composition.

The composition may have the same composition as a commercial EPDM rubber wherein as the paraffinic oil the Fischer-Tropsch derived process oil is present. Examples of commercial EPDM rubbers are the Keltan® EPDM
30 rubbers from DSM Elastomers, the Vistalon® EPDM rubbers from ExxonMobil Chemical and Dutral® EPDM rubbers from Enichem.

The composition may also be a thermoplastic vulcanisate composition comprising an ethylene-propylene-diene rubber component and a poly-olefin component. The poly-alpha olefin is preferably polypropylene. Such compositions combines the elastic properties of a rubber with the processing characteristics of a thermoplast. The composition comprises preferably EPDM particles embedded in a polypropylene (PP) matrix. The PP phase presents the processing behavior of a PP, while the cured EPDM rubber provides excellent elastic properties. The composition may have the same composition as a commercial TPE composition, wherein as the paraffinic oil the Fischer-Tropsch derived process oil is present. Example of commercial thermoplastic vulcanisate are the Keltan®EPDM or Sarlink®TPV series from DSM Elastomers.

The below example will illustrate the preparation of a Fischer-Tropsch process oil having the desired properties for use in a composition according to the invention.

Example 1

The C₅-C₇₅₀ °C⁺ fraction of the Fischer-Tropsch product, as obtained in Example VII using the catalyst of Example III of WO-A-9934917, was continuously fed to a hydrocracking step (step (a)). The feed contained about 60 wt% C₃₀⁺ product. The ratio C₆₀⁺/C₃₀⁺ was about 0.55. In the hydrocracking step the fraction was contacted with a hydrocracking catalyst of Example 1 of EP-A-532118. The effluent of step (a) was continuously distilled under vacuum to give lights, fuels and a residue "R" boiling from 370 °C and above. The yield of gas oil fraction on fresh feed to hydrocracking step

was 43 wt%. The properties of the gas oil thus obtained are presented in Table 3.

The main part of the residue "R" was recycled to step (a) and a remaining part was sent to a catalytic dewaxing step (c). The conditions in the hydrocracking step (a) were: a fresh feed Weight Hourly Space Velocity (WHSV) of 0.8 kg/l.h, recycle feed WHSV of 0.25 kg/l.h, hydrogen gas rate = 1000 Nl/kg, total pressure = 40 bar, and a reactor temperature of 335 °C.

In the dewaxing step, the fraction described above boiling from 370 °C to above 750 °C was contacted with a dealuminated silica bound ZSM-5 catalyst comprising 0.7% by weight Pt and 30 wt% ZSM-5 as described in Example 9 of WO-A-0029511. The dewaxing conditions were 40 bar hydrogen, WHSV = 1 kg/l.h and a temperature of 365 °C.

The dewaxed oil was distilled into a process oil fraction boiling above 510 °C and a fraction boiling below said fraction. The yield of process oil based on feed to dewaxing step was 27.9 wt%. The process oil (Process oil-1) was analyzed in more detail and the properties are listed in Table 1.

Example 2

A Shell MDS Waxy raffinate was contacted with a dealuminated silica bound ZSM-5 catalyst comprising 0.7% by weight Pt and 30 wt% ZSM-5 as described in Example 9 of WO-A-0029511. The dewaxing conditions were 40 bar hydrogen, WHSV = 1 kg/l.h and a temperature of 345 °C.

The dewaxed oil was distilled into a process oil fraction (Process oil 2) boiling having an initial boiling point as 466 °C and a 90 wt% boiling point of 567 °C. The yield of process oil on waxy raffinate feed

was 12.3 wt%. Other properties of thye process oil are listed in Table 1.

Table 1

	Process oil-1	Process oil-2
density at 20 °C	837.0	831.5
pour point (°C)	+9	-39
kinematic viscosity at 40 °C (cSt)		56.6
kinematic viscosity at 100 °C (cSt)	22.92	9.1
VI	178	139
sulphur content (%w)	< 0.001	< 0.001
Flash point (°C) (ISO 2592)	> 300	276
UV absorption at 300 nm (ASTM D 2008-A1)	< 0.6	< 0.6
Evaporation loss at 107 °C after 22 hours (ASTM D 972)	< 0.05	< 0.05
CN number (IEC 590)	Not measu red	18.6

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1. Composition comprising a ethylene-propylene-diene rubber component and a Fischer-Tropsch derived process oil.

2. Composition according to claim 1, wherein the
5 Fischer-Tropsch derived oil has a flash point of above 260 °C.

3. Composition according to any one of claims 1-2, wherein the UV adsorption of the process oil at 300 nm is less than 0.6% according to ASTM D 2008-A1.

10 4. Composition according to any one of claims 1-3, wherein the evaporation loss of the process oil at 107 °C during 22 hours is less than 0.05 wt%.

5. Composition according to any one of claims 1-4, wherein the kinematic viscosity at 100 °C of the process
15 oil is greater than 8 cSt.

6. Composition according to any one of claims 1-5, wherein the pour point of the process oil is below 10 °C.

7. Composition according to claim 6, wherein the process oil has a pour point of below 10 °C and a kinematic
20 viscosity at 100 °C of above 9 cSt.

8. Composition according to any one of claims 1-7, wherein the process oil is obtained by

(a) hydrocracking/hydroisomerisating a feed comprising a Fischer-Tropsch synthesis product;

25 (b) isolating from the product of step (a) a process oil precursor fraction,

(c) dewaxing the process oil precursor fraction obtained in step (b) to obtain the process oil, optionally after

separating a lower boiling fraction from said dewaxed product.

9. Composition according to claim 8, wherein step (c) is performed by solvent dewaxing.

5 10. Composition according to claim 8, wherein step (c) is performed by catalytic dewaxing.

11. Composition according to any one of claims 8-10, wherein the conversion in step (a) is between 25 and 70 wt%.

10 12. Thermoplastic vulcanisate composition according to any one of claims 1-11, wherein the composition comprises a Ethylene-propylene-diene rubber component and a poly-olefin component.

15 13. Thermoplastic vulcanisate composition according to claim 12, wherein the poly-olefin is polypropylene.

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COMPOSITION COMPRISING EPDM AND A PARAFFINIC OIL

Composition comprising a ethylene-propylene-diene rubber component and a Fischer-Tropsch derived process oil. The process oil preferably has a flash point of above 260 °C and an evaporation loss at 107 °C during 22 hours of less than 0.05 wt%.

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